Voronoi Fluid Particle Dynamics

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November 17, 2009

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- Introduction
 - Fluid Dynamics
 - Computational FD
 - Euler vs Lagrange
- Pluid particle dynamics
 - Fluid particles
 - Smoothed particle hydrodynamics
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 - The gradient
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• a very classical theory

- Some names:
 - Bernoullis (Johann, Daniel
 - Gauss
 - Stokes
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 - Lorentz! From wikipedia: In the years 1918-1926, at the request of the Dutch government, Lorentz headed a committee to calculate some of the effects of the proposed Afsluitdijk (Closure Dike) flood control dam on other seaworks in the Netherlands. ... Lorentz proposed to start from the basic hydrodynamic equations of motion and solve the problem numerically. ... One of the two sets of locks in the Afsluitdijk was named after him.

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The Laws of Fluid Dynamics

Continuity (aka, matter or charge conservation):

$$\frac{\partial \rho}{\partial t} = -\operatorname{div} \rho \mathbf{v}$$

Notation

div
$$\mathbf{v} \equiv \nabla \cdot \mathbf{v} = \sum_{\alpha=1,2,3} \frac{\partial v_{\alpha}}{\partial x_{\alpha}}$$

grad
$$p \equiv \nabla p$$
; (grad $p)_{\alpha} = \frac{\partial p}{\partial x_{\alpha}}$

$$abla^2 \mathbf{v} \equiv \Delta \mathbf{v}; \quad (
abla^2 \mathbf{v})_lpha = \sum_{eta = 1, 2, 3} rac{\partial^2 v_lpha}{\partial x_eta^2}$$

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Laws: Navier-Stokes equations

Continuity:

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Momentum density ρv_{α} , for each coordinate $\alpha = 1, 2, 3$:

$$\frac{\partial \rho \mathbf{v}_{\alpha}}{\partial t} = -\operatorname{div} \rho \mathbf{v}_{\alpha} \mathbf{v} - \frac{\partial p}{\partial x_{\alpha}} + \eta \nabla^2 \mathbf{v}_{\alpha} + \frac{\eta}{3} \frac{\partial}{\partial x_{\alpha}} \operatorname{div} \mathbf{v}$$

Entropy density *s* (this, we will largely neglect today):

$$\frac{\partial s}{\partial t} = -\operatorname{div} s \mathbf{v} + 2\eta \overline{\nabla \mathbf{v}} : \overline{\nabla \mathbf{v}} + \kappa \nabla^2 T$$

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Computational FD

CFD: The hard task of computing numerical solutions to these *non-linear* equations.



From ENSIGHT

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Euler's view

Use a grid, and finite differences (or finite elements) for equations that are written in this "frame". E.g., Continuity:

$$rac{\partial
ho}{\partial t} = -\operatorname{div}
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FEM mesh of human heart (Zhang et al. 2004)

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Problems arise in many situations.

- When one does not know in advance where more effort (CPU and RAM) will be needed (turbulence, astrophysics...)
- When the boundary is also moving, "free boundary problems". E.g. surface waves (what people call "waves"!).

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Gate opening in a tank with a wet bed (SPHERIC test case) SPH (Spartacus-2D, EDF R&D) vs experiments (Janosi ct a/., 2004)

From SPHERIC website

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From SPHERIC website

This calls for a *Lagrangian* approach, and computational methods that will be either *meshless* or have a *moving* $mesh_{p, n} \in \mathbb{R}$

E.g., continuity:

$$\frac{\partial \rho}{\partial t} = -\operatorname{div} \rho \mathbf{v}$$

means

$$\frac{\partial \rho}{\partial t} + (\mathbf{v} \nabla) \rho = -\rho \operatorname{div} \mathbf{v}$$

... but this is

$$\frac{D\rho}{Dt} = -\rho \operatorname{div} \mathbf{v},$$

where D/Dt is the substantive derivative: how things change as they flow! **Notation:** $D\rho/Dt \equiv d\rho/dt \equiv \dot{\rho}$

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Lagrangian coordinates

They are defined by pathlines:

$$rac{\partial \mathbf{R}(\mathbf{r},t)}{\partial t} = \mathbf{v}(\mathbf{R}(\mathbf{r},t),t),$$

with initial condition $\mathbf{R}(t=0) = \mathbf{r}$.

As a valid transformation, it has a Jacobian J, which can be shown to satisfy

$$\frac{DJ}{Dt} = J \operatorname{div} \mathbf{v}.$$

So, it looks like an infinitesimal *volume* that is carried by the flow (e.g., this would be the equation for $v = 1/\rho$).

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Since it looks like a volume, lets call it so: V = J. We may introduce extensive particle

- mass $M = \rho V$
- momentum $\mathbf{P} = \rho \mathbf{v} V$
- entropy S = sV

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The resulting equations are

$$\begin{aligned} \frac{\partial \mathbf{R}}{\partial t} &= \mathbf{v} \\ \hline \frac{\partial \rho}{\partial t} &= -\operatorname{div} \rho \mathbf{v} & \frac{DM}{Dt} &= 0 \\ \hline \frac{\partial v_{\alpha}}{\partial t} &= -\operatorname{div} \rho v_{\alpha} \mathbf{v} - \frac{\partial p}{\partial x_{\alpha}} + \eta \dots & \frac{1}{V} \frac{DP_{\alpha}}{Dt} &= -\frac{\partial p}{\partial x_{\alpha}} + \eta \dots \\ \hline \frac{\partial s}{\partial t} &= -\operatorname{div} s \mathbf{v} + \eta \dots & \frac{1}{V} \frac{DS}{Dt} &= 0 + \eta \dots \end{aligned}$$

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Other forms for the momentum eq.

These will be important later

$$\frac{1}{V}\frac{DP_{\alpha}}{Dt} = -\frac{\partial p}{\partial x_{\alpha}} + \eta \nabla^2 v_{\alpha} + \frac{\eta}{3}\frac{\partial}{\partial x_{\alpha}} \operatorname{div} \mathbf{v}$$

$$\frac{1}{V}\frac{DP_{\alpha}}{Dt} = -\frac{\partial p}{\partial x_{\alpha}} + \eta \sum_{\beta} \frac{\partial \sigma_{\alpha\beta}}{\partial x_{\beta}},$$

with

$$\sigma_{\alpha\beta} = \left(\frac{\partial v_{\alpha}}{\partial x_{\beta}} + \frac{\partial v_{\beta}}{\partial x_{\alpha}}\right) - \frac{2}{3}\delta_{\alpha\beta}\operatorname{div}\mathbf{v}.$$

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With vectors,

$$\frac{1}{V}\frac{D\mathbf{P}}{Dt} = -\operatorname{grad} p + \eta \operatorname{Div} \sigma,$$

Just remember: there is a grad involved in the reversible part, and a Div in the irreversible (viscous) part.

Also, for weak compressions this may suffice:

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Fluid particles

Recall the Lagrangian approach, without a fixed mesh.

- The fluid is described by a set of moving nodes moving according to the velocity field (*convection* is very well described).
- Physically, these are *fluid particles*, a classic concept
- Particles are small subsystems that are, nevertheless large for thermodynamics. (No "particle physics"!).
- If they are quite small (\sim 100 molecules), thermal fluctuations can (and should) be included



Figure 7. Fluid particle travelling along a curved streamline.

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Particles SPH VP

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Computational particles

Given a set of point, what are the corresponding fluid particle? Two methods have been proposed



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Smoothed particle hydrodynamics

Rather well established method that does not use any meshes.

Particles are "smooth", since their properties depend on all other within the range (support) of a weight function. For example, the density of a particle depends on its "neighbours"

(the more, the denser), and the volume is its inverse (the more, the smaller).



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Voronoi particles

The volume of a particle, V_i , is the one of its Voronoi cell.

The Delaunay triangulation is its dual — the particles are the vertices.

This way, "neighbours" are perfectly defined.



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The first equations of motion are easy enough:

$$\frac{\partial \mathbf{R}}{\partial t} = \mathbf{v} \qquad \Rightarrow \qquad \dot{\mathbf{R}}_i = \mathbf{v}_i$$
$$\frac{DM}{Dt} = 0 \qquad \Rightarrow \qquad \dot{M}_i = 0$$

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But: the rest involve (many!) space derivative operators: grad p, Div σ ...

$$\frac{1}{V}\frac{D\mathbf{P}}{Dt} = -\operatorname{grad} p + \operatorname{Div} \sigma \qquad \Rightarrow \qquad \frac{1}{V_i}\dot{\mathbf{P}}_i = -(\operatorname{grad} p)_i + (\operatorname{Div} \sigma)_i$$

The main task:

To find expressions for each of these, at particle *i*, in a "Voronoi discrete vector calculus"! (or, "Delaunay DVC").

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Recall the equation for the particle volume (aka Jacobian):

$$rac{DV}{Dt} \equiv \dot{V} = V \operatorname{div} \mathbf{v}.$$

Translated to particles:

$$\dot{V}_i = V_i (\operatorname{div} \mathbf{v})_i$$

But, the chain rule tells us

$$\dot{V}_i = \sum_j rac{\partial V_i}{\partial \mathbf{R}_j} \dot{\mathbf{R}}_j = \sum_j rac{\partial V_i}{\partial \mathbf{R}_j} \mathbf{v}_j.$$

Comparing the two:

$$(\operatorname{div} \mathbf{v})_i \doteq \frac{1}{V_i} \sum_j \frac{\partial V_i}{\partial \mathbf{R}_j} \mathbf{v}_j.$$

(Note: it's actually Div, but it has the same expression.),

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What is the change of V_i w.r.t. \mathbf{R}_i ? It can be shown that

$$\frac{\partial V_i}{\partial \mathbf{R}_j} = A_{ij} \left(\frac{\mathbf{u}_{ij}}{2} - \frac{\mathbf{c}_{ij}}{R_{ij}} \right).$$

A_{ij} is the area of the facet between i and j
u_{ij} is the unit vector from i to j
c_{ii} is the vector to the c.o.m. of the facet



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What is the change of V_i w.r.t. \mathbf{R}_i ? It can be shown that

$$\frac{\partial V_i}{\partial \mathbf{R}_j} = A_{ij} \left(\frac{\mathbf{u}_{ij}}{2} - \frac{\mathbf{c}_{ij}}{R_{ij}} \right)$$

- A_{ii} is the area of the facet between i and j
- **u**_{ij} is the unit vector from *i* to *j*
- c_{ii} is the vector to the c.o.m. of the facet



We may therefore write:

$$(\operatorname{div} \mathbf{v})_i = \frac{1}{V_i} \sum_{j \neq 1} A_{ij} \left[\frac{\mathbf{u}_{ij}}{2} - \frac{\mathbf{c}_{ij}}{R_{ij}} \right] \cdot (\mathbf{v}_j - \mathbf{v}_i),$$

which "looks" very nice indeed.



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This is a bit harder. We may begin with the total internal energy

$$E = \sum_{i} \frac{1}{2} M_i v_i^2 + \epsilon(\{V_i\}).$$

Let's make sure it does not change:

$$\dot{E} = \sum_{i} \left(M_i \mathbf{v}_i \dot{\mathbf{v}}_i - p_i \dot{V}_i \right) = 0.$$

(Yes, the pressure $p_i = -\partial \epsilon / \partial V_i$.) We saw before

$$\dot{V}_i = \sum_j \frac{\partial V_i}{\partial \mathbf{R}_j} \mathbf{v}_j.$$

Therefore

$$\dot{E} = \sum_{i} M_{i} \mathbf{v}_{i} \dot{\mathbf{v}}_{i} - \sum_{i} p_{i} \sum_{j} \frac{\partial V_{i}}{\partial \mathbf{R}_{j}} \mathbf{v}_{j} = 0.$$

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D. Duque

Voronoi Fluid Particle Dynamics

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We may then choose

$$M_i \dot{\mathbf{v}}_i = \sum_j \frac{\partial V_j}{\partial \mathbf{R}_i} p_j$$

But, remember the (reversible) momentum equation

$$M_i \dot{\mathbf{v}}_i = -V_i \,(\text{grad } p)_i$$

This gives us:

$$(\operatorname{grad} p)_i \doteq -\frac{1}{V_i} \sum_j \frac{\partial V_j}{\partial \mathbf{R}_i} p_j$$

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The gradient

We may therefore write (after some tidying up):

$$(\operatorname{\mathsf{grad}} p)_i = rac{1}{V_i} \sum_{j \neq i} A_{ij} \left[rac{\mathbf{u}_{ij}}{2} \left(p_i + p_j \right) - rac{\mathbf{c}_{ij}}{R_{ij}} \left(p_i - p_j \right)
ight].$$



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The gradient: good news

- $(\operatorname{grad} p)_i = 0$ at all *i* if *p* is constant
- (grad p)_i = a at all i if p = a ⋅ r: linear fields have the right gradient!
- The grad operator shows nice convergence, as h^2 for regular lattices, and h^1 for random meshes.



The divergence: bad news

Despite its nice appearance, this div operator convergences as h^1 for regular lattices, and h^0 for random meshes (not at all!).



D. Duque Voronoi Fluid Particle Dynamics

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The divergence issue

The div appears as soon as we include viscosity — we first have to evaluate the stress tensor σ :

$$\sigma_{\alpha\beta} = \left(\frac{\partial \mathbf{v}_{\alpha}}{\partial x_{\beta}} + \frac{\partial \mathbf{v}_{\beta}}{\partial x_{\alpha}}\right) - \frac{2}{3}\delta_{\alpha\beta}\operatorname{div}\mathbf{v}.$$

We can expect problems since the divergence of tensor σ appears:

$$\frac{1}{V}\frac{D\mathbf{P}}{Dt} = -\operatorname{grad} p + \eta \operatorname{Div} \sigma,$$

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The divergence issue: a way out

For small compression, we only need the Laplacian

$$\frac{1}{V}\frac{DP_{\alpha}}{Dt} = -\frac{\partial p}{\partial x_{\alpha}} + \eta \nabla^2 \mathbf{v}.$$

Is there an alternative way to approximate it? Sure there is: the finite element method!

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The Laplacian is very well studied in the FEM. The steps would be

- From the existing Delaunay triangulation (which is actually very good for the FEM)
- On each node *i* define a pyramid-like weight function Φ_i, with value 1 at the node, 0 at the neighbours, and constant slope in each incident face (triangle)

These elements discretize continuous fields:

$$\mathbf{v}_i = rac{1}{\mathcal{V}_i} \int \Phi_i(\mathbf{r}) \mathbf{v}(\mathbf{r})$$

• \mathcal{V}_i is the integral of Φ_i . We term it the "Delaunay volume": 1/(D+1) of the sum of the areas of the incident triangles



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$$\mathbf{v}(\mathbf{r}) \approx \sum_{j} v_{j} \Phi_{j}(\mathbf{r}).$$

$$(\nabla^2 \mathbf{v})_i = -\sum_j v_j \frac{1}{\mathcal{V}_i} \int \nabla \Phi_i \nabla \Phi_j \equiv \frac{1}{\mathcal{V}_i} \sum_j \Delta_{ij} v_j$$

$$\Delta_{ij} = \left(\cot\theta + \cot\theta'\right)/2,$$



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The integral may be evaluated for each pair of nodes. In 1D, one gets the well-known $x_{i-1} + x_{i+1} - 2x_i$. In 2D:

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Our approach to hydrodynamics is then at two levels:

- For the reversible (Euler) part of the dynamics, just use Voronoi concepts (Voronoi volume, formula for grad...)
- For the irreversible (viscous) part, use Delaunay concepts and a FEM expression for the Laplacian (optionally, other features).

Why not use the second approach everywhere? Simply because the Delaunay volume makes sudden jumps on rearrangements. Not nice at all for the particle volume, tolerable for the force.

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Create initial points, momenta, pressures

- 2 Build a Delaunay triangulation
- O Calculate info for vertices and edges
- Apply changes in positions and momenta (Verlet algorithm, predictor-corrector...):

$$\dot{\mathbf{R}}_i = \mathbf{v}_i = \mathbf{P}_i / M_i$$

 $rac{1}{V_i} \dot{\mathbf{P}}_i = -(\operatorname{div} p)_i + \eta (\nabla^2 \mathbf{v})_i.$

Either:

- just update all positions and go to 2, or
- update positions one by one, restoring the Delaunay condition, and go to 3.

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Standard hydrodynamic benchmarks: Confined fluids

- Couette flow
- Poiseuille
- Vortex spin-down
- Lamb-Oseen vortex

Not-so-standard benchmarks: Periodic bc

- Kolmogorov flow
- Taylor-Green flow



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Not-so-standard benchmarks: Periodic bc

- Kolmogorov flow
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Applications

Not-so-standard benchmarks: **Periodic bc**

- Kolmogorov flow
- Taylor-Green flow



"Real" applications: Free surfaces

- Elliptical drops
- Dam breaking
- Sloshing

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Other ideas:

• "Delaunay particles" everywhere?

- Centroidal Voronoi tessellation
- Natural coordinates vs FEM interpolation
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- U. Oslo: Eirik G Flekkøy
- The workshop organizers
- The kind audience

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Some references

- Pep Español and Ignacio Zúñiga, for the Delaunay volume and the Laplacian
- Pep Español and Mar Serrano, in "Tessellations in the Sciences Virtues, Techniques and Applications of Geometric Tilings", Eds: Rien van de Weijgaert, Gert Vegter, Jelle Ritzerveld, and Vincent Icke, Kluwer/Springer (2009)
- A good source is Pep Español's references webpage

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